# Integrated Data-Driven Framework for Automatic Controller Tuning with Setpoint Stabilization Through Reinforcement Learning

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- Keywords: Simulation-Based Optimization, Automatic Controller Tuning, Bayesian Optimization, Time Series Clustering, Online Learning, Reinforcement Learning, Setpoint Stabilization.
- Abstract: We introduce a three-stage framework for designing an optimal controller. First, we apply offline black-box optimization algorithms to find optimal controller parameters based on a heuristically chosen setpoint profile and a novel cost function for penalizing control signal oscillations and direction changes. Then, we leverage cloud data to generate device-specific setpoint profiles and tune the controller parameters to perform well on the device with respect to the same cost function. Finally, we train a control policy on top of the offline tuned controller after deployment on device through an online learning algorithm to handle unseen setpoint variations. A novel reward function encouraging setpoint stabilization is added for preventing destabilization from coupling effects. Bayesian Optimization and Nelder-Mead methods are used for offline optimization, and a state-of-the-art model free Reinforcement Learning algorithm namely Soft Actor-Critic is used for online optimization. We validate our framework using a realistic HVAC hydraulic circuit simulation.

# **1 INTRODUCTION**

Proportional integral derivative (PID) controllers are at the core of a majority of control systems deployed to this date owing to their simple design and robust performance. However, they need adequate tuning to perform effectively thus encouraging the development of manual and automatic tuning strategies (Ziegler and Nichols, 1993; Cohen and Coon, 2022; Garcia and Morari, 1982; Åström and Hägglund, 2004). With the formulation of PID tuning as an optimization problem, modern optimization, data-driven, and machinelearning (ML) based techniques saw widespread success due to their proficiency in handling general nonconvex objective functions (Gaing, 2004; Ahmad et al., 2021; Mok and Ahmad, 2022).

These data-driven techniques rely on repeated simulations and offline data collection. This leads to limited generalizability since the offline-data may not capture all probable model operating points. For example, in Heating, Ventilation, and Cooling (HVAC) systems typical temperature setpoints vary with seasons and geographical regions. Furthermore, in hierarchical PID control systems, extremely non-linear interactions between the subsystems cannot be captured easily by offline tuning algorithms again necessitating large-datasets which are expensive to collect. These concerns led to development of data-driven control algorithms which can adapt to changing conditions online. The most notable methods are data-driven predictive control (Zhuang et al., 2023) and reinforcement learning (RL) (Sutton and Barto, 2020).

RL is able to optimize general objectives without any assumptions on convexity, differentiability, and sparsity of the objective function. However, it relies on learning by randomly exploring the feasible control input space which can destabilize the system if deployed directly. Therefore, it is preferable to deploy RL on top of a known suboptimal but stabilizing base controller like PID as explored in (Solinas et al., 2024). But if the underlying PID controller is poorly tuned, the overall system will continue to behave poorly until RL learns to take optimal actions, which takes quite some time in practice due to model free RL's low sample efficiency (Recht, 2018). Therefore, one should tune the base PID gains to the best possible values based on the model information and empirical data available at hand using the mentioned offline tuning strategies. To the best of our knowledge, no existing work explores this fusion of offline tuned controllers and online learning control policies.

In this paper, we introduce an optimization framework for data driven automatic controller tuning employing three sequential stages of optimization. First,

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we utilize black-box optimization methods to tune a controller within a simulation to optimally follow a heuristically chosen setpoint profile. Then, we leverage cloud collected data to tune controllers to device specific setpoint profiles while ensuring that we do not overfit the controller parameters to the training data and generalize well to new and unseen setpoint profiles. Finally, an additional parameterized control law is added to the offline optimized control law. This new parameter set is learned online to adapt to unknown setpoint profiles and unknown couplings between the cascaded feedback loops. We add setpoint stabilization as a key objective for learning an improved controller online since in the online setting one can explicitly compensate for the effects of coupling by learning the influence of control actions on the setpoint. We validate the framework using a realistic HVAC system simulation and show that adding the online learning policy significantly improves tracking performance compared to just using the offline tuned controllers.

The paper is organized as follows: Section 2 summarizes the related work. Section 3 presents the overall idea of the proposed optimization framework followed by details on the offline optimal, and online learningbased control. In Section 4, we use experimental results to showcase the advantages of the proposed methodology. Finally, Section 5 discusses conclusions and directions for future investigations.

# 2 RELATED WORK

Applying BO for controller tuning was recently explored in (Neumann-Brosig et al., 2020) and (Fiducioso et al., 2019). In (Neumann-Brosig et al., 2020) the evaluations are done based on real-time laboratory experiments, which require a corresponding infrastructure that makes the tests time- and resourceconsuming. Furthermore, the paper (Fiducioso et al., 2019) estimates different optimal control parameters depending on the outside air temperatures, which are then used for gain scheduling. However, the study does not consider the influence of setpoints profile variations on controller performance. This oversight highlights the need for research considering various setpoint profiles which could be crucial for optimizing the controller's performance in practical scenarios.

On the other hand, several recent works on HVAC control systems have focused on online learning based control. These solutions often rely on RL algorithms to learn policies that optimize for energy use, cost, comfort, etc. To highlight a few, (Yu et al., 2020) learn a radial basis function neural network policy using DQN (Mnih et al., 2013). They rely on a well tuned PI



Figure 1: Data driven framework for controller parameter optimization.

controller for the policy to collect experience samples. Other methods such as (Solinas et al., 2024; Esrafilian-Najafabadi and Haghighat, 2023) use transfer learning to find a good initial control policy for online RL. Online system identification, as is done in (Hazan et al., 2018) to learn a feedforward controller online would also be applicable to our framework. These works support our idea that a systematic and data-driven approach to finding an optimal controller requires the controller to be adaptive to its specific environment. Furthermore, these works illustrate the success of online learning controllers in HVAC systems.

# 3 A FRAMEWORK FOR OPTIMAL AND LEARNING BASED CONTROL

In this section, we introduce a model-free framework for automated data-enabled controller tuning (Figure 1). In particular, we do not make any assumptions on the dynamics of the system. The framework is defined as three-stage process consisting of offline controller optimization on heuristic setpoint profiles (1a, 1b), offline controller optimization on data driven generated setpoint profiles (2a, 2b), and learning an adaptive controller online with setpoint stabilization (3). Heuristic setpoint profiles (1a) are manually chosen generic setpoint profiles representing the common variation of setpoints expected for a given control device across different applications. While of the other hand, one can collect time series information over long periods of time from a particular device in the field. Taking the example of an HVAC device like a control valve for ventilation circuits, this data will contain setpoints profiles that vary with slowly evolving external variables like seasons, pipe insulation changes, etc. Thus, for device specific tuning we use a clustering algorithm to group similar setpoint profiles. We can then use these clusters to sample device specific, field



Figure 2: Schematic of closed-loop black-box optimization.

realistic setpoint profiles, and this is what we refer to as *clustered setpoint profiles* throughout this paper.

In stage 1, we optimize the controller performance (1b) over the heuristically chosen setpoint profile (1a), while in stage 2 (2a-2b) we use a generated clustered setpoint profile for the same. One can directly start by optimizing on the clustered profiles, but since the output of stage 1 is a general tuning which can serve as a foundation to warm-start the optimizer, we refer to device specific tuning as stage 2. Doing so, we ensure optimal performance in their specific application. In stage 3 we add an online learning component to the offline tuned controller for adaptive control. We can also use the optimization results after each step without going through all optimization steps successively; however, having the initial offline optimal controller provides a stable base controller which can be leveraged by the learning-based controller for safe exploration. Removing the learning-based controller does not allow adaption to uncertain environments. Therefore, all the three stages are complimentary to each other.

#### 3.1 Offline Optimization

We illustrate the black-box offline optimization in Figure 2. It uses a closed-loop simulation consisting of a complex plant and an internal controller. The dynamics of the plant are assumed to be unknown to the controller. Let r(t) denote the setpoint to the internal controller, y(t) denote the observations from the system. Then we denote the parameterized controller as  $u(t) = f(r(t), y(t), \theta)$  with parameters  $\theta$ . The goal of the black box optimizer is to find the optimal controller parameters  $\theta^*$  that minimize a performance based objective function  $J(\theta)$  calculated in the closedloop simulation. This objective function is calculated over the duration of a setpoint profile and appears as an oracle model to the black-box optimization routine.

In this work, the controller performance metric is formulated as a multi-objective optimization problem as shown in Equation (1). Where  $\omega_1, \omega_2, \omega_3, \omega_4$  are the weights for each term,  $e_{\text{control}}(t)$  is the control error, and  $e_{\text{oscillation}}(t) = e_{\text{control}}(t)$  during the oscillations and 0 otherwise. u(t) is the parameterized controller as defined before, and D(t) is the number of sign changes of the first derivative of the control signal u(t). The first term is the Integral Time-weighted Absolute Error (ITAE) (Stenger and Abel, 2022) and is chosen to penalize overshoots. The second term is calculating the total variation of controller output and is selected to minimize oscillations in the control signal. The third term is the ITAE measured during oscillations, and final term ensures that we minimize the direction changes due to sharp tuning of controller:

$$J(\theta) = \omega_1 \int |te_{\text{control}}(t)| dt$$
  
+  $\omega_2 \int |u(t+1) - u(t)| dt$   
+  $\omega_3 \int |te_{\text{oscillation}}(t)| dt$   
+  $\omega_4 \int D(t) dt$  (1)

By minimizing Equation (1) over controller parameters  $\theta$  we achieve the best balance between optimal setpoint tracking, minimal controller movements and oscillations.

For finding optimal controller parameters using a sophisticated simulation, only black-box optimization methods apply, since differentiating the objective in Equation (1) with respect to the controller parameters is intractable. Furthermore, the performance evaluation of each parameter configuration requires a simulation run, which may be computationally expensive. Therefore, we choose BO in our framework, as it is particularly suitable to cases where evaluation of the objective is expensive. While BO excels at finding minima across a broad non-convex search space, it might not get as close as desirable to the identified minimum. Hence, we use BO to identify a promising region in the search space and refine the result using the Nelder-Mead simplex algorithm afterward.

We use a Radial Basis Function kernel added to a white kernel for Gaussian Process regression with the Upper Confidence Bound acquisition function. A detailed treatment of BO can be found in (Rasmussen and Williams, 2005). To further improve the controller performance, we employ the Nelder-Mead simplex optimization method (Gao and Han, 2012) and initialize with the best parameters found by BO.

#### **3.2** Data Driven Controller Optimization

Thus far, we assume that the controllers' performance is evaluated on a simulation using a heuristically chosen setpoint profile. This may lead to overfitting since the final controller parameters may be optimal for the heuristically chosen setpoint profile, but suboptimal when the device is used in the real world. Since more and more devices are connected to the cloud and make their setpoint data available to system integrators and device manufacturers, we additionally analyse historical data of controller setpoint signals to further enhance the suitability of the optimal parameters to real-world applications. We aim to optimize the controller parameters of each device for its specific environment. To this end, we need to identify typical device specific setpoint profiles and then tune the controller parameters while avoiding overfitting. We employ the following steps to overcome this issue:

- Data preprocessing followed by dimensionality reduction of the setpoint profiles using an autoencoder.
- 2. Clustering the samples in the latent space of the autoencoder. The cluster centers represent the most typical example of each setpoint profile cluster.
- 3. Choosing the two setpoint profiles closest to the cluster center for each cluster, one to be used for training and one for testing.
- 4. Applying the optimization method of the previous section to the training set to obtain controller parameters. Check if the final controller also performs well on the test set and keep them if that is the case.

We will now elaborate on the details of steps 1-3.

### 3.2.1 Data Preprocessing & Dimensionality Reduction

The cloud data may be just one long setpoint time series that spans over multiple years. The best preprocessing method depends on the device and application. We suggest splitting up the data by day and ensuring that all samples are of equal length, such that the previous assumption holds. One way to achieve this is by splitting the cloud data up by day and cropping or padding the samples such that we obtain a dataset with samples of equal length.

We expect that there is a set of unknown factors that lead to several classes of setpoint profiles that share some similarities within each class. Hence, we want to reduce the dimensionality such that only informative dimensions are kept. Downstream, the clustering algorithms will primarily operate on informative data, which leads to more informed clustering. We use standard autoencoders in our approach (Goodfellow et al., 2016).

**Autoencoders:** are artificial neural network architectures that learn a mapping from high dimensional data to a low dimensional representation as well as an inverse mapping. We define two mappings  $f_{\theta} : \mathbb{R}^n \to \mathbb{R}^c$ 

and  $g_{\phi} : \mathbb{R}^k \to \mathbb{R}^n$  where the encoder with parameters  $\theta$  by is denoted by  $f_{\theta}$  and the decoder with parameters  $\phi$  is denoted by  $g_{\phi}$ . The data dimension is *n* and the latent dimension of the encodings is *c* and we assume that  $n \ll c$ . In general terms, we can take a sample  $\mathbf{x} \in \mathbb{R}^n$  and use the encoder to get a low dimensional representation  $\mathbf{z} = f_{\theta}(\mathbf{x})$ . We can approximately recover the input sample  $\mathbf{x} \approx \tilde{\mathbf{x}} = g_{\phi}(\mathbf{z})$ . The autoencoder is trained by minimizing the reconstruction error

$$\mathcal{L}^{(\mathrm{AE})}(\mathbf{X}, \boldsymbol{\phi}, \boldsymbol{\theta}) = \frac{1}{n} \sum_{i=1}^{n} \left\| \mathbf{x}^{(i)} - f_{\boldsymbol{\theta}} \left( g_{\boldsymbol{\phi}}(\mathbf{x}^{(i)}) \right) \right\|_{2}^{2}.$$
 (2)

The mathematical program is given by

$$\boldsymbol{\theta}^*, \boldsymbol{\phi}^* = \operatorname*{arg\,min}_{\boldsymbol{\theta}, \boldsymbol{\phi}} \left\{ \mathcal{L}^{(AE)}(\mathbf{X}, \boldsymbol{\theta}, \boldsymbol{\phi}) \right\}. \tag{3}$$

We train an autoencoder on the real world setpoint profiles to get encodings  $\mathbf{z}^{(i)} = f_{\theta} \left( \mathbf{x}^{(i)} \right)$ . We minimize the mathematical program in Equation (3) using the Adam optimizer. Once the encodings are obtained, we can proceed with clustering.

#### 3.2.2 Centroid Clustering

Next we find representative setpoint profiles by clustering the latent encodings  $\mathbf{z}^{(i)}$ . Let  $k \in \mathbb{N}_+$  denote the number of setpoint profile types. Clustering techniques in general group the input samples into k subsets such that the distances within clusters are minimized according to some measure. Centroid based methods proceed by finding k cluster centers such that the distances to the centroids are minimized for each corresponding subset. We use the classic k-means algorithm (MacQueen, 1965) for setpoint profile clustering.

**Choosing Setpoint Profiles for Parameter Optimization.** The goal of our framework is to find controller parameters systematically and avoid overfitting to specific setpoint profiles. To this end we follow a standard approach in machine learning. We construct a training set and a test set. The training set is used by the optimization procedure to find the optimal controller parameters. The test set is used only in the end to check that the controllers still perform well on new, unseen setpoint profiles.

For each cluster we select the two samples that are nearest to their respective cluster center, and add one sample to the train set and the other sample to the test set. We chose the BO hyperparameters manually as outlined in Section 3.1 and found them to be satisfactory; therefore, we did not perform hyperparameter optimization.

# 3.3 Learning Based Online Adaptive Control & Setpoint Stabilization

At this point, we have a controller which is optimally tuned based on whatever existing knowledge and data we had collected from the system. But in practical scenarios the controller device may be subjected to unprecedented scenarios for which the existing tuning may be suboptimal. In this section, we'll consider the example of a real HVAC system and motivate the requirement for an online learning component as the final stage of the framework presented.

Figure 3 depicts the block diagram of a hydraulic circuit based air supply temperature control system for indoor heating and cooling systems. The external controller, which can be a room temperature control unit, receives a temperature setpoint  $r_e(t)$  from the user and translates it to desired flow rate  $r_i(t)$  for a heating/cooling fluid flowing through the hydraulic circuit. This flow setpoint is sent to a control valve, referred to as the internal controller, with an actuator attached to the hydraulic circuit. Controlling the flow rate controls the amount of heat transferred through the heat exchanger, thus controlling the outlet temperature as a result. The heat exchanger's dynamics is very hard to model and is often unknown.

Observe that the error in temperature tracking  $(e_e(t))$  is directly affected by the valve, which means that the control signal of the valve actually has an unknown coupling relationship with the external controller and; therefore, with its own setpoint. Therefore, it is possible for the controller to destabilize the setpoint itself. Furthermore, time varying field conditions, diverse hydraulic circuit setups across different environments and other external factors can introduce uncertainties which render the offline optimized parameters suboptimal. These limitations highlight the inadequacy of offline controller optimization alone and underscores the need for an adaptation strategy to effectively tackle the challenges of dynamic environments. This adaptation is achieved in data-driven manner through online learning.

We achieve this by augmenting the offline learned control law  $f(r_e(t), y_e(t), \theta^*)$  with an online learned control policy  $g(r_i(t), \tilde{y}(t), \phi)$ , henceforth referred to as the auxiliary controller. The terms  $f(\cdot), \theta^*$  were defined in Section 3.1, and  $\phi, \tilde{y}(t)$  represent the parameters and input observations of the auxiliary controller for this and the following sections. Note that  $\tilde{y}(t)$ is multidimensional and contains informative signals like the flow meter feedback  $y_i(t)$ , the flow tracking error  $e_i(t)$ , and much more depending on the auxiliary controller design. Since in this paper it represents information obtained from the hydraulic circuit, it is



Figure 3: Block diagram of a cascaded control loop for temperature control.

illustrated as data flowing from the hydraulic circuit to the RL agent in Figure 3. The final control signal from the internal controller can be expressed as:

$$u(t) = f(r_e(t), y_e(t), \boldsymbol{\theta}^*) + g(r(t), \tilde{y}(t), \boldsymbol{\phi}).$$
(4)

#### 3.3.1 Optimization Objective & Setpoint Stabilization

To learn the control policy g online, we need to define an objective to minimize for the online learning algorithm. RL works in a discrete-time control setting and requires a stage cost definition much similar to that of model predictive control. To retain the performance objectives discussed in Section 3.3.1, the following stage cost is considered

$$J_k(\phi) = \lambda_1 \|e_k\|_2 + \lambda_2 F_{\text{osc},k} + \lambda_3 F_{\text{dir},k} + \lambda_4 J_{\text{set},k}(\phi)$$
<sup>(5)</sup>

where  $e_k$  is the tracking error at time step k, and  $\lambda_i$  for  $i = 1, \dots, 4$  are the weights of each cost component. The functions  $F_{\text{osc},k}$  and  $F_{\text{dir},k}$  are defined as follows

$$F_{\text{osc},k} = \begin{cases} 1 & \text{if actual flow is oscillating at time } k, \\ 0 & \text{otherwise} \end{cases}$$
(6)

$$F_{\text{dir},k} = \begin{cases} 1 & \text{if } \dot{u}(t) \text{ changed sign at time } k, \\ 0 & \text{otherwise} \end{cases}$$
(7)

where  $\dot{u}(t)$  denotes the first order time derivative of the control signal. These functions penalize the control policy if it tries to make too many direction changes, or makes the flow through the control valve oscillate.  $J_{\text{set},k}(\phi)$  is a term added to enforce setpoint stability.

Setpoint stability in this case is viewed in the sense of how quickly the setpoint varies with time. Therefore, we quantify the variation in setpoint signal and use it as the penalty term. Let  $r_{ref,t}$  denote the desired setpoint signal at time t, a straightforward choice for quantifying variation is to use the magnitude of the first and second-order derivatives of the reference signal:  $\left\|\frac{d}{dt}r_{\text{ref},t}\right\|_p$ , and  $\left\|\frac{d^2}{dt^2}r_{\text{ref},t}\right\|_p$ , where  $\|\cdot\|_p$  denotes the *p*-norm of some vector.

In our experiment we use the 2-norm of the first order finite difference approximation for the derivative and use Equation (8) as the penalty term.

$$J_{\text{set},t}(\phi) = \|r_{\text{ref},t} - r_{\text{ref},t-1}\|_2$$
 (8)

Among all available approaches for online learning we choose RL for its capability to handle arbitrary reward functions through policy search algorithms. In this paper we use the Soft-Actor Critic (SAC) RL algorithm (Haarnoja et al., 2018) which is currently state-of-the-art. Due to its off-policy nature SAC is sample efficient. Furthermore, SAC maximizes the entropy of the action policy which ensures that the policy does not place all probability mass on a single action in some states leading to better exploration and regularization in policy updates.

The central goal of RL is to find a control policy that minimizes the discounted infinite horizon expected cost at a given time step t

$$J(\phi) = \sum_{k=t}^{\infty} \gamma^{k-t} J_k(\phi).$$
(9)

where  $\gamma$  denotes the discount factor and is a commonly used notation in RL literature. Note that the time weighing of the ITAE terms is captured through  $F_{\text{osc},k}$ and  $F_{\text{dir},k}$  but a constant penalty of 1 is used instead of the errors to ensure that the policy gradients do not take unbounded values to ensure numerical stability. For ensuring stable policies we keep *gamma* close to 1 (Recht, 2018). The exact definition of the overall cost optimized by SAC is stated in Appendix A of (Haarnoja et al., 2019). For an in-depth treatment of reinforcement learning, we refer the reader to (Sutton and Barto, 2020).

### **4 EXPERIMENTAL RESULTS**

The aim of our experimental evaluation is to demonstrate the successful application of the presented model-free offline tuning and online adaptation controller framework to a realistic scenario. We considered the outlet temperature control system from Figure 3 and implemented it in the MATLAB<sup>®</sup> Simulink<sup>®</sup> simulation environment. We modeled a water hydraulic circuit which controls the temperature of air supplied through the heat exchanger at the outlet using an isothermal valve. For custom component modelling of the hydraulic circuit and the heat-exchanger we used the Simscape<sup>®</sup> modelling language (The MathWorks Inc., 2024). The heat-exchanger we used in this work is modelled according to (Fux et al., 2023). The heat exchanger and other simulated models, including the isothermal valve, the hydraulic circuit pipes, fluid intake reservoirs, etc. were verified to match with their real-world counterparts. Refer to Section 3.3 for a brief description of the control problem.

The actuator position is specified in the range of [0,1] where 0 denotes completely closed and 1 denotes fully open. The external controller is a PI controller which takes the error in outlet temperature and gives a relative water flow setpoint to the valve (internal controller). For the physical definition of relative water flow, the reader is referred to (Zhang et al., 2022).

The offline optimization with BO and Nelder-Mead is implemented in python. We call Simulink<sup>©</sup> to execute the simulation and obtain the objective values, which are then passed back to the optimizer in python. Setpoint profile dimensionality reduction and clustering is also implemented in Python and then exported to Simulink for validation. Details on the RL implementation follow in Section 4.3.

# 4.1 Automated Tuning with Heuristic Setpoint Profiles

This section introduces the results obtained during offline optimization with empirically derived heuristic profiles as shown in Figure 1 (part 1).

As an initial step in our optimization process we had to identify the optimal weights for Equation (1). To balance the contribution of each design objective in this cost function, we defined an additional objective function that scales each component by its corresponding weight and aims to minimize the variance among the scaled components. See the Appendix for detailed results. We used these aligned weights to guide both the initial and subsequent optimization phases. By minimizing the variance of the scaled components, we made sure that no design objective dominated and ensured that the optimization process can explore the parameter space. This optimization progress is shown in Figure 4a.

Figure 4b illustrates further modification of the parameters due to Nelder-Mead. Although this development does not have a strong impact on our objective function, it shows that our algorithm is searching towards potential better values to further minimize our non-penalized terms of objective function.

The optimized controller's performance on the heuristic stepwise setpoint profile, as illustrated in Figure 4c demonstrates stable setpoint tracking with low response times and no oscillations.



Figure 4: *Experimental results, heuristic setpoint profile.* (a) Progress of objective function during optimization. (b) Progress of tuning parameters. (c) Controller performance after optimization on a heuristic setpoint profile.

# 4.2 Automated Tuning with Clustered Setpoint Profiles

In this section we present our results from applying black-box optimization on clustered setpoint profile as discussed in Section 3.2. The first step involves clustering of typical setpoint profiles collected over a year. We use a single fully connected layer for both the encoder and decoder neural networks. We refer the reader to the appendix for a description of the autoencoder and its training setup. Here the combination of 4000 epochs and a dimensionality of 4 yielded the best results (see Figure 11a and Figure 11b). We calculate the optimal number of clusters by applying grid search using the silhouette score. Figure 5a shows the improvement in the cost function with optimization steps.

In Figure 5b the progress of the controller parameters is illustrated. Especially noticeable is the further optimization towards a minimum during the Nelder-Mead phase. After the final optimization of the parameters, the performance of the controller on a clustered setpoint profile is shown in Figure 5c.

Furthermore, to examine how well these parameters generalize, we test them on our clustered setpoint signal generated for the testing phase. The flow tracking results shown in Figure 6 demonstrate satisfactory tracking performance.

## 4.3 Reinforcement Learning

This section presents the results attained by applying SAC, by directly connecting it to the hydraulic circuit simulation in closed-loop feedback. We do not assume any form of pre-training on the actor model since our objective is to demonstrate that a suitably exploring RL policy such as SAC can learn to control the flow setpoint in an online setting. Therefore, our configuration corresponds to the *scratch* configuration of online RL as described in (Zhang et al., 2023).

The objective function from Equation (5) was im-

plemented using standard blocks and functions in Simulink. For implementing RL, we used the Reinforcement Learning Toolbox<sup>©</sup> from MATLAB<sup>®</sup> (The MathWorks Inc., 2024). Due to the toolbox being specifically suited for episodic RL instead of online RL, we carried out the experiments in the episodic setting. However, note that demonstrating successful learning and control performance through episodic learning is equivalent to proving it in the online setting. This is because the algorithm employed is an off-policy RL strategy that updates the policy network at every step of the environment episode by uniformly sampling a minibatch of data from a circular experience buffer. In fact, if we just assume that the initial condition of every new episode is the exact same as where the previous episode ended, then the chain of episodes is indistinguishable from online learning. It is because of this reason that time weighing is not considered for the oscillation error term, otherwise, this equivalence to online RL will no longer hold. One important distinction between episodic and online learning is that when the episodes start with a random initial condition the samples from episodic learning cover a large portion of the distribution since random explorations in online learning can only be in the neighborhood of the current state. Thus episodic learning in this sense may lead to faster convergence to the optima.

The RL agent is integrated with the system such that its actions are added to the base PI flow controller's signal according to Equation (4). This addition allows the base PI controller to act like a pre-stabilizer to the system when the initially untrained SAC policy behaves like white noise making sure that the system doesn't exhibit dangerous behavior. Note that the base PI controller parameters are obtained from the offline optimization step, and for this experiment, we used heuristic setpoint profiles.

The set of observations to the RL agent comprised of the current error, the current setpoint, and the current control input calculated by the base PI controller. To allow the agent to learn to predict the system dynamics, and to make sure it receives the full set of



Figure 5: *Experimental results, clustered setpoint profile.* (a) Progress of objective function during optimization. (b) Progress of tuning parameters. (c) Controller performance after optimization on a clustered profile from the training set.



Figure 6: Controller performance after optimization on a clustered profile from the test set.

information due to the non-markovianity induced by non-linearities like deadzones and stiction, we also feed the last 4 observations as input to the actor and the critic networks. The base PI controller's output is given as an input in order to allow the RL agent to learn its trends and make adjustments to yield an overall optimal signal. Finally, note that the mean of the actor distribution is allowed to be in the range of [-1,1] to allow it to completely modify the PI flow controller's control signal which lies in the range of [0,1]. A saturation function is applied to the final control signal from Equation (4) to restrict it in the valid range of [0,1].



Figure 7: Episode reward trend along with the average return.

Figure 7 shows the trend of the variation in total cost throughout the episode. It can be observed that the algorithm improves rapidly in the initial episodes and then seems to plateau when it cannot learn further based on the information provided. Being an entropy maximizing algorithm one observes consistent gradual improvement even after 160 episodes (approx. 2.8M samples).

Figure 8 shows the comparison between the closed loop control response of the trained and untrained SAC agents, demonstrating the improvement in setpoint tracking performance as training progresses. A comparison between the setpoint tracking performance of the offline optimized PI flow controllers and the controller with the online optimized RL agent added to it is shown in Figure 9. The error signal fed to the RL and the PI controller encounters a deadzone near the zero-point. This non-linearity leads to the error being zero near the setpoint which is why the RL agent doesn't get penalized for small oscillations. The direction change and oscillation terms make up for this shortcoming and lead to gradual improvement in removing oscillatory behavior by the agent. See the Appendix for the SAC hyperparameters configuration and the actor-critic network architectures used in the experiments.

#### OGY PUBLICATIONS

# 5 CONCLUSION

In this paper, we presented a data-driven model-free framework for automatic controller tuning and online adaptation with setpoint stabilization in coupled systems. We experimentally demonstrated that our approach works on realistic scenarios in unknown systems with undetermined coupling relationships and is, therefore, applicable to a broad range of practical systems. We also showed that the last step of further optimizing the controller online to its specific environment is crucial to obtain a better performing controller.

Our example of a cascaded control system is omnipresent in HVAC systems, and is applicable to a large variety of systems encountered in control systems design. It is well known that such systems of cascaded controller configurations quickly become unstable and traditional solutions which rely on adjusting their time-constants to differ by an order of magnitude are not optimal. We believe that the notion of learning to stabilize the control setpoint and minimize a cost function with online learning is a key ingredient



(a) Agent after episode 2. (b) Agent after episode 137.

Figure 8: Setpoint tracking performance comparison of the RL agent at different phases in the training. The labels mention the number of episodes the agent has been trained for. Observe how the agent first learns to minimize the error and eventually reduces the number of actuator oscillations. Each plot shows the supply air temperature tracking the temperature setpoint (top) and the flow setpoint with the actual water flow (bottom). In all cases the trained trained policy is still sampling actions from the random distribution.



Figure 9: Setpoint tracking performance comparison of the controllers obtained after the 3 different stages. The RL agent is operating on top of the clustered profile trained PI flow controller. Note that the currently used setpoint profile is quite different from the ones considered for the PI base controller in stages 1 and 2. The training profiles were changing stepwise for which the PI controllers learned to converge as fast as possible without oscillations due to Equation (1). Thus, they are too sharply tuned for the smooth and continuous flow stepoint they receive from the temperature controller which leads to the oscillations observed in (a) and (b). The RL agent adapts to this new unseen profile and, therefore, performs better than the offline optimized parameters after being trained online as can be seen in (c) which validates the requirement for online learning.

towards optimal control and adaptation in an online setting. We do not claim that our combination of algorithms for each step of the framework is the best, since there are several more combinations of offline and online policies learned through other strategies which may be better. However, this work is an important step towards achieving optimal online adaptive control and presents a new paradigm for data-driven controller design.

#### 5.1 **Future Work**

For this work, we applied our optimization on a simulated hydraulic circuit without any variations. To

achieve a more generalized final solution, we plan to introduce variations into our plant and expand our scope by exploring other application types, such as air or refrigeration applications.

This work trained an RL agent from scratch by applying it directly to the system in a closed loop setting. It is worth exploring other strategies such as actor-critic pre-training on base controller data before gradually deploying the RL Policy as done in (Solinas et al., 2024). Furthermore, several strategies like imitation learning on offline data, policy expansion of offline trained policies by bridging them with online trained policies, etc. are worth exploring as discussed in (Zhang et al., 2023).

The problem of instability in cascaded controllers also extends to the setting of networked control systems. To take an example from the setting presented in this paper, oftentimes several temperature control units send flow setpoints to multiple flow control valves which are connected to the same hydraulic circuit and thus have unknown physical coupling effects between each other thus rendering any single-agent control law suboptimal and potentially destabilizing. It may thus be interesting to learn the physical dependencies of the cascaded controllers and leverage this information to stabilize such controller networks. This directly leads the research in the direction of multi-agent reinforcement learning. We propose to continue research on these ideas and extend the framework we present in this work accordingly.

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## APPENDIX

#### **SAC Hyperparameters**

Table 1 lists the hyperparameter configuration used for training the Soft-Actor critic agent mentioned in Section 4.3.

#### **Actor-Critic Networks**

Figure 10 shows the neural-network architectures used for the actor and the critic networks. The observation input to the critic network (Figure 10a) is 15 dimensional since the set of observations at a given time-step consists of 3 scalars, and we feed the last 4 observations along with the current time-step to both the networks. In the actor net (Figure 10b) tanh layer is used to allow the mean action to be in [-1, 1] to allow full range modification of the base PI flow controller's signal, while a softplus layer is used to ensure positive values for the standard deviation of the action distribution.



Figure 10: SAC actor and critic neural network architectures.

# **Bayesian Optimization, Clustering and Autoencoder Training**

The optimized weights for different setpoint profiles are shown in Table 2.

#### **Autoencoder Networks**

The autoencoder consists of an encoder network and a decoder network. For both networks we choose simple one layer neural networks. The encoder has the

Table 1: SAC hyperparameter conf	iguration.
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Parameter	Value
Optimizer	Adam (Kingma and
	Ba, 2017)
Learning rate	0.001
Discount factor ( $\gamma$ )	0.99
Minibatch size	256
Entropy target	$-1(-\dim(\mathcal{A}))$
Target smoothing coeff. $(\tau)$	0.001
Target update frequency	1
Policy update frequency	1
Gradient steps	1
Replay buffer size	10 <sup>5</sup>
Number of warm start steps	1810
Episode length	1800
Number of episodes	126
Simulation time step	0.1 sec
$(\lambda_1,\lambda_2,\lambda_3,\lambda_4)$	$10^{-2} \cdot (6, 1.6, 1, 0.1)$

Weight	Heuristic Set- point Profile	Clustered Setpoint Profile
Weight 1	1.11777344	1.20485840
Weight 2	2.24179687	2.09331055
Weight 3	704.68750	1082.29980
Weight 4	3036.91406	2000.00000

Table 2: Optimized weights for different setpoint profiles.

Table 3: Autoencoder training hyperparameters.

Parameter	Value
Optimizer	Adam
Learning Rate	$10^{-4}$
$\beta_1$	0.9
$\beta_2$	0.999
Batch size	64
Epochs	3000
Loss Function	Mean Squared Error

following structure

1. Fully Connected Layer (1000  $\rightarrow$  4)

```
2. ReLU
```

And the decoder has a similar architecture

- 1. Fully Connected Layer (4  $\rightarrow$  1000)
- 2. Sigmoid

The hyperparameters used for training are listed in Table 3.

#### Clustering

See Figure 11a and Figure 11b.



Figure 11: (a) Validation losses of last epoch for different latent dimensions. (b) Training and validation losses over epochs.